

2014
**Membrane
Technology**
CONFERENCE & EXPOSITION



NOVEL ULTRAFILTRATION OPERATING PROCESS FOR SILICON WAFER PRODUCTION WASTEWATER REUSE

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American Water Works
Association

The Authoritative Resource on Safe Water®

America's Authority in Membrane Treatment



American Membrane Technology Association

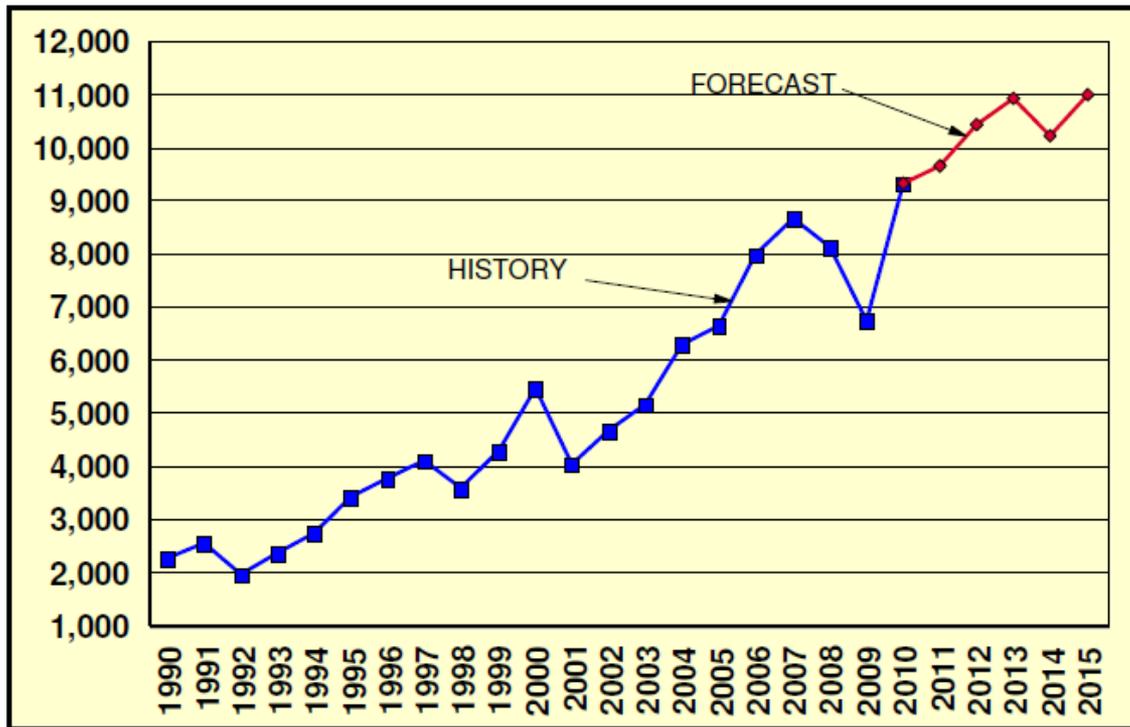
Improving America's Waters Through Membrane Treatment and Desalting

Outline

- Introduction
- Case Study 1
- Case Study 2
- Conclusions

Introduction

SEMICONDUCTOR SILICON WAFER FORECAST



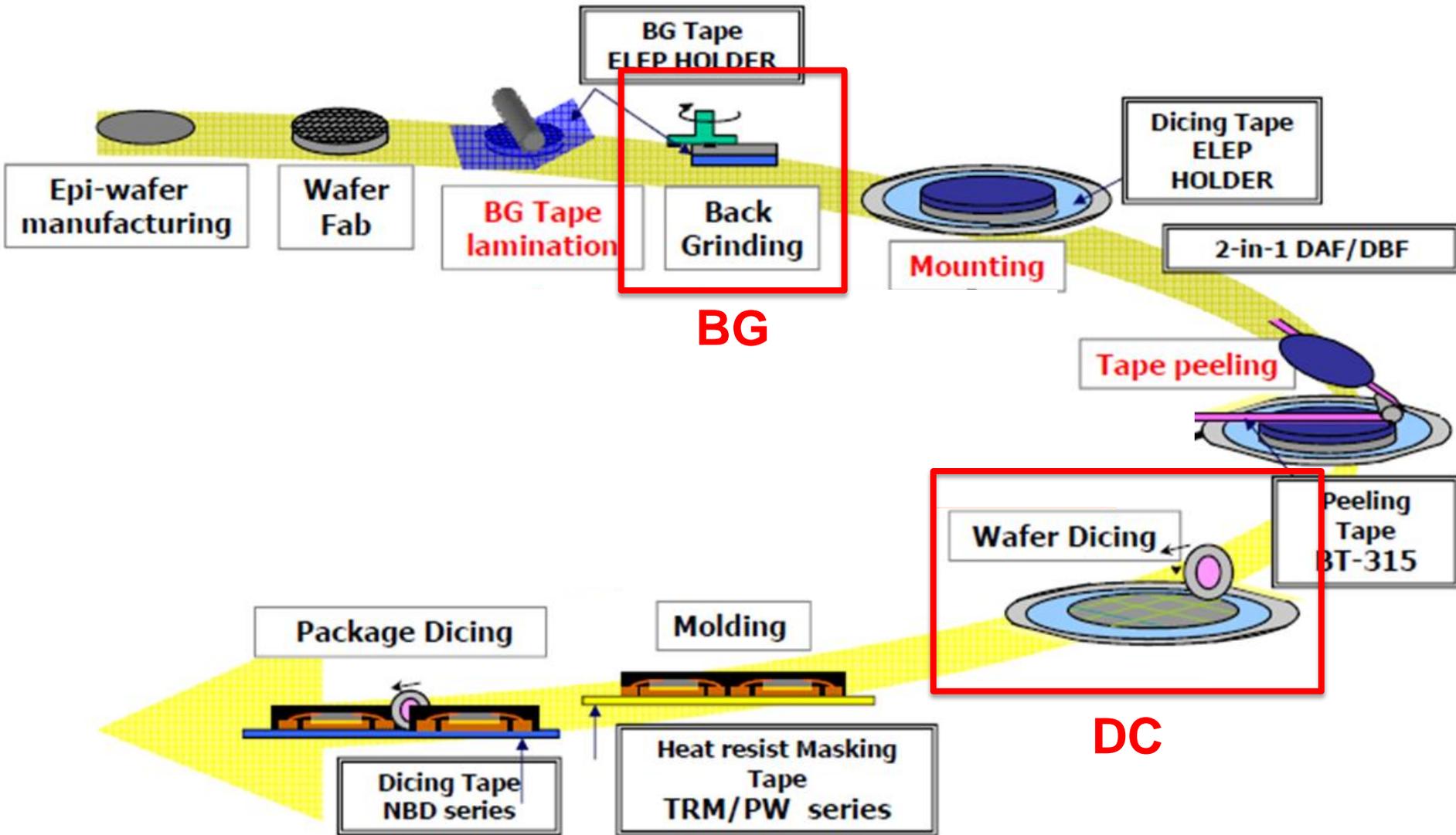
GLOBAL SILICON WAFER SALES FORECAST IN MILLIONS OF SQUARE INCHES

Source: Sage Concepts Market Report

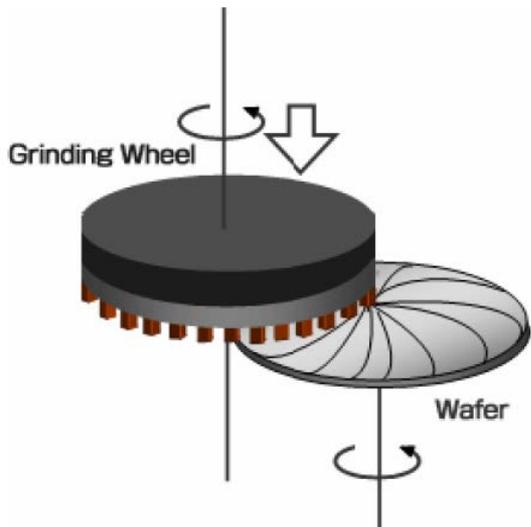
- **2010 Water Consumption = 450 MGD***
- **2015 Projected Water Consumption = 533 MGD***

* Assumes production of single 300 mm silicon wafer requires ~2000 gallons of water.

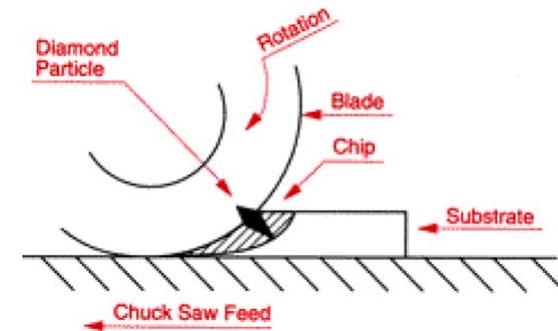
Semiconductor Manufacturing Process (Back side)



Back grinding (BG) and Dicing (DC)



Backgrinding + Dicing WW (left) and Dicing WW only (right)



Source: www.adt-dicing.com

Source: GRINDING OF SILICON WAFERS: WAFER SHAPE MODEL AND ITS APPLICATIONS (Sun, 2005)

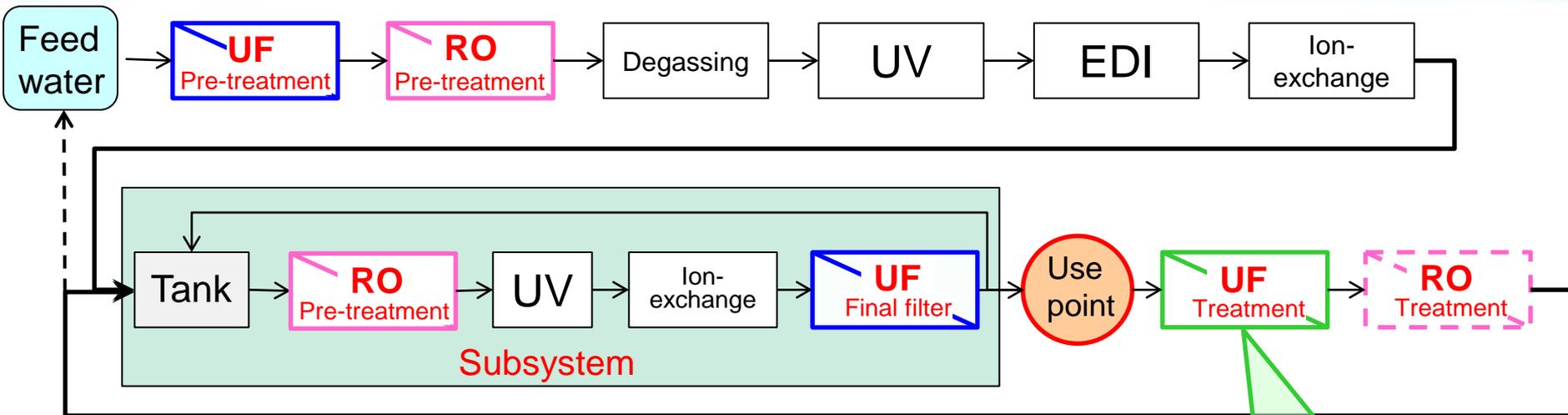
Back grinding WW Characteristics

Particle Size (μm)	0.1 - 0.3
Turbidity (NTU)	>1,000

Dicing WW Characteristics

Particle Size (μm)	0.2 - 2
Turbidity (NTU)	>100

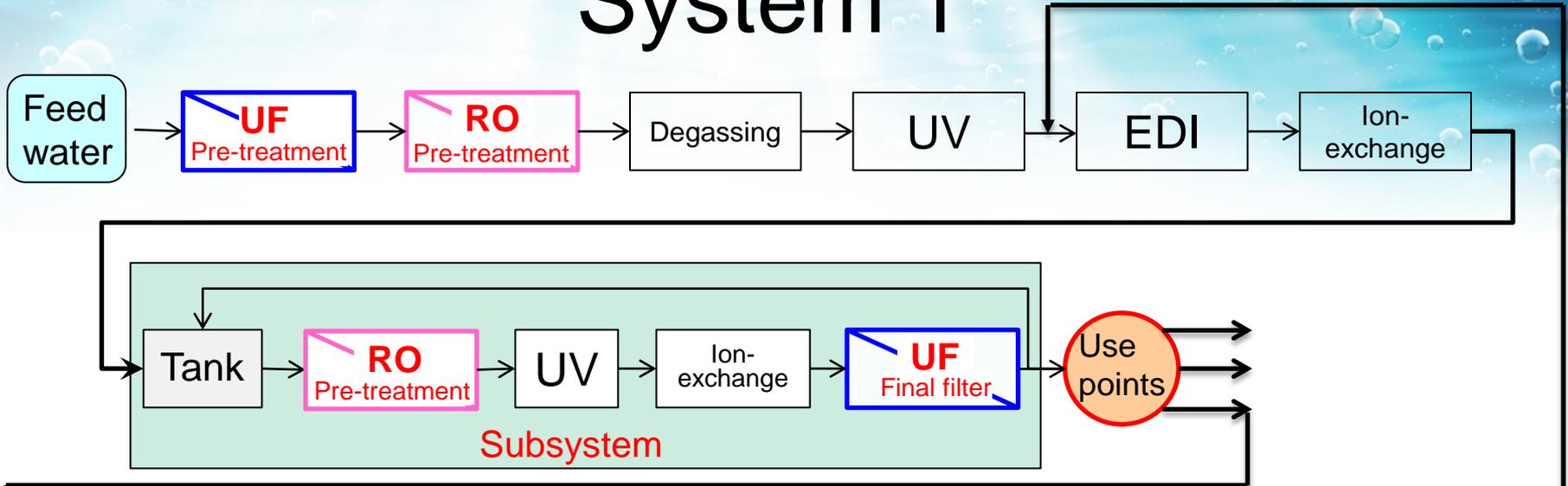
Ultrapure Water Process



- Reduction of source water consumption results in:
 - Lower source water and wastewater disposal cost
 - Potential reduction in primary treatment system sizing

BG/DC
wastewater
recycle/reuse

System 1



BG/DC WW
Only



200 micron
Filter



System 1

Parameter	Unit	Value
System capacity	m3/hr	15
Module type		Hydranautics HYDRAcap® MAX 60
Number of racks		1
Number of modules per rack		6
Gross operating filtration flux	LMH	32
Concentrate bleed flow	m3/hr	1.5
Filtration cycle duration	min	45
Physical cleaning method		Air scour without backwash
Air scour flow rate per module	m3/hr	4
Chemical cleaning frequency		Two 0.1% NaOH maintenance cleans per day
System Recovery	%	90

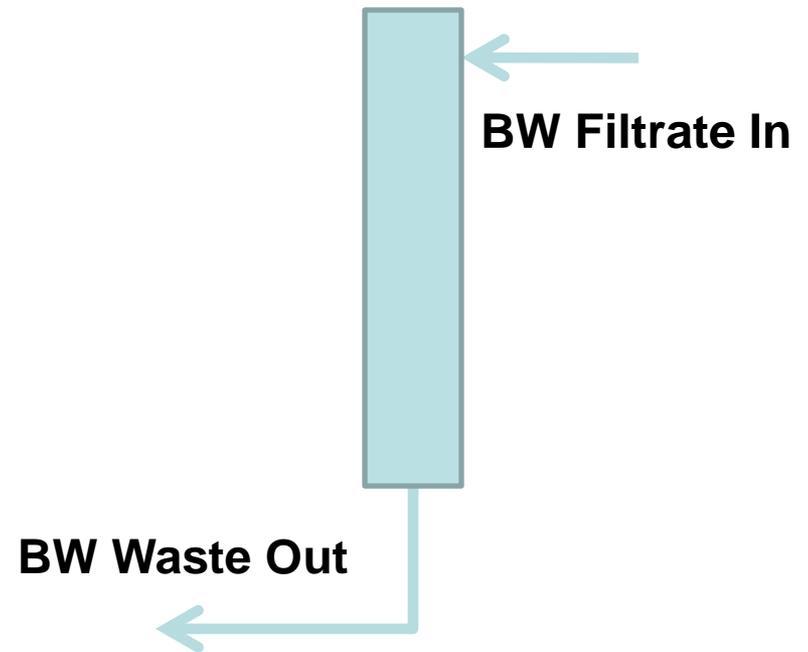
HYDRAcap® MAX 60 Overview

Flow path	Outside to inside
Membrane material	TIPS PVDF
Membrane configuration	Hollow fiber
Membrane area	840 ft ² (78 m ²)
Fiber ID/OD	0.6/1.2 mm
Pore size	0.08 µm



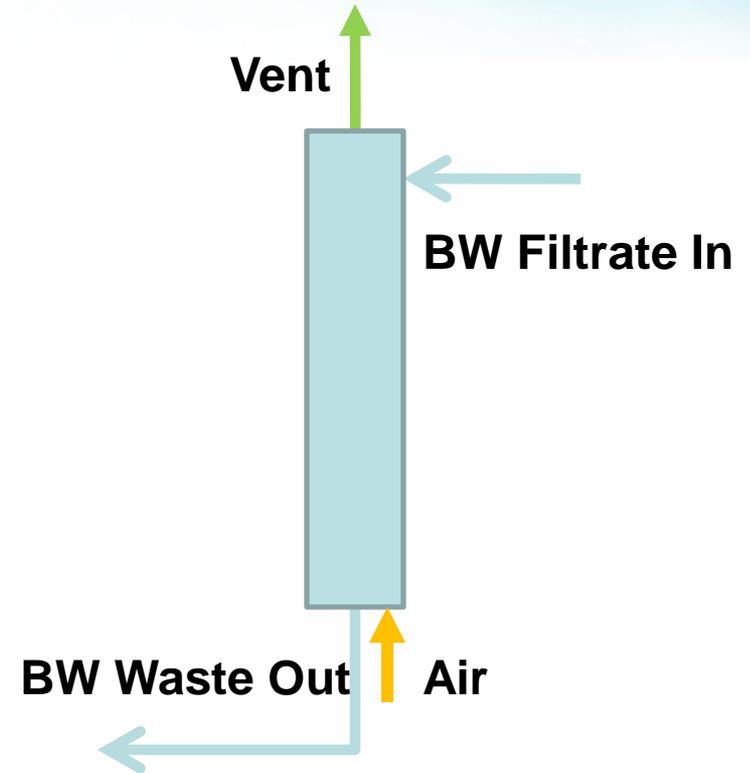
Physical Cleaning Methods

1. Backwash



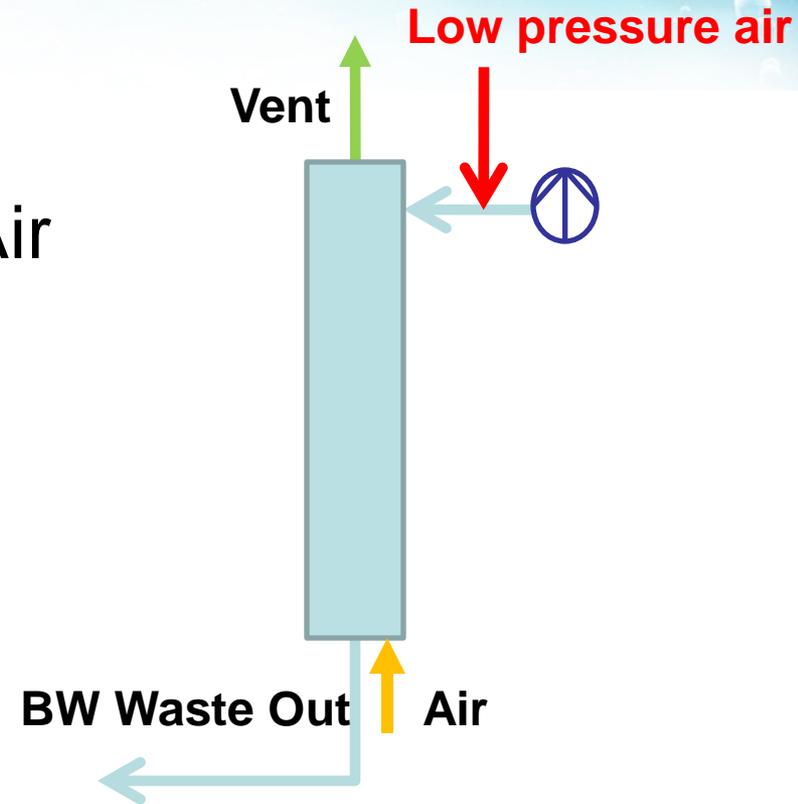
Physical Cleaning Methods

1. Backwash
2. Backwash + Air Scour



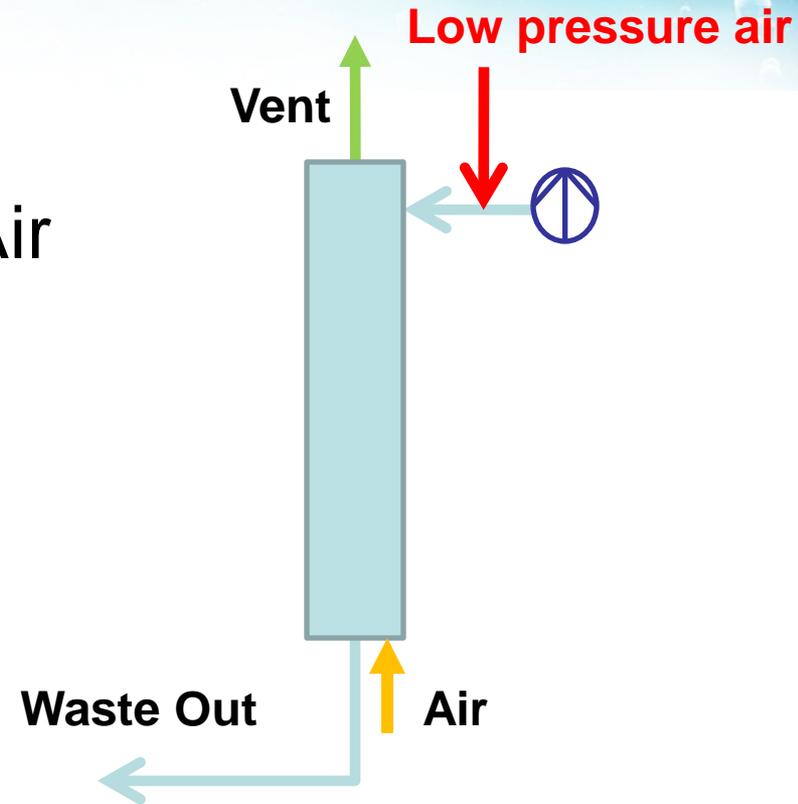
Physical Cleaning Methods

1. Backwash
2. Backwash + Air Scour
3. Air Assisted Liquid BW + Air Scour



Physical Cleaning Methods

1. Backwash
2. Backwash + Air Scour
3. Air Assisted Liquid BW + Air Scour
4. Air Scour



System 1 – Physical Cleaning Process

	Air Scour Step	Typical Duration (s)
1	Stop Filtration	0
2	Air Scour	60
3	Air Scour and Drain	60
4	Refill	60
5	Resume Filtration	0



System 1 – Physical Cleaning Process

	Air Scour Step	Typical Duration (s)
1	Stop Filtration	0
2	Air Scour	60
3	Air Scour and Drain	60
4	Refill	60
5	Resume Filtration	0

Air flow: 12 – 15 m³/h per module
 Air pressure: 0.7 bar



System 1 – Physical Cleaning Process

	Air Scour Step	Typical Duration (s)
1	Stop Filtration	0
2	Air Scour	60
3	Air Scour and Drain	60
4	Refill	60
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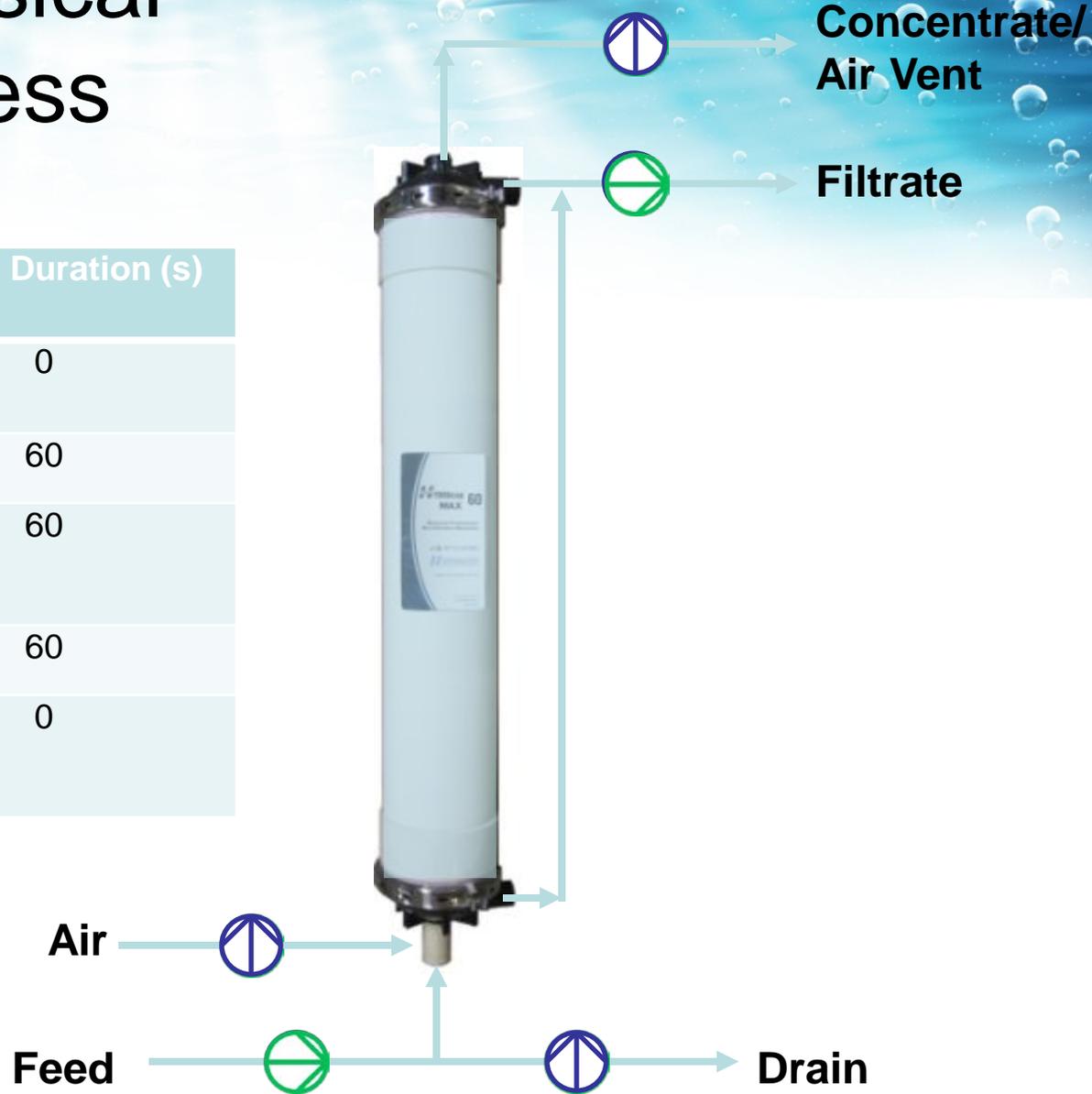
System 1 – Physical Cleaning Process

	Air Scour Step	Typical Duration (s)
1	Stop Filtration	0
2	Air Scour	60
3	Air Scour and Drain	60
4	Refill	60
5	Resume Filtration	0

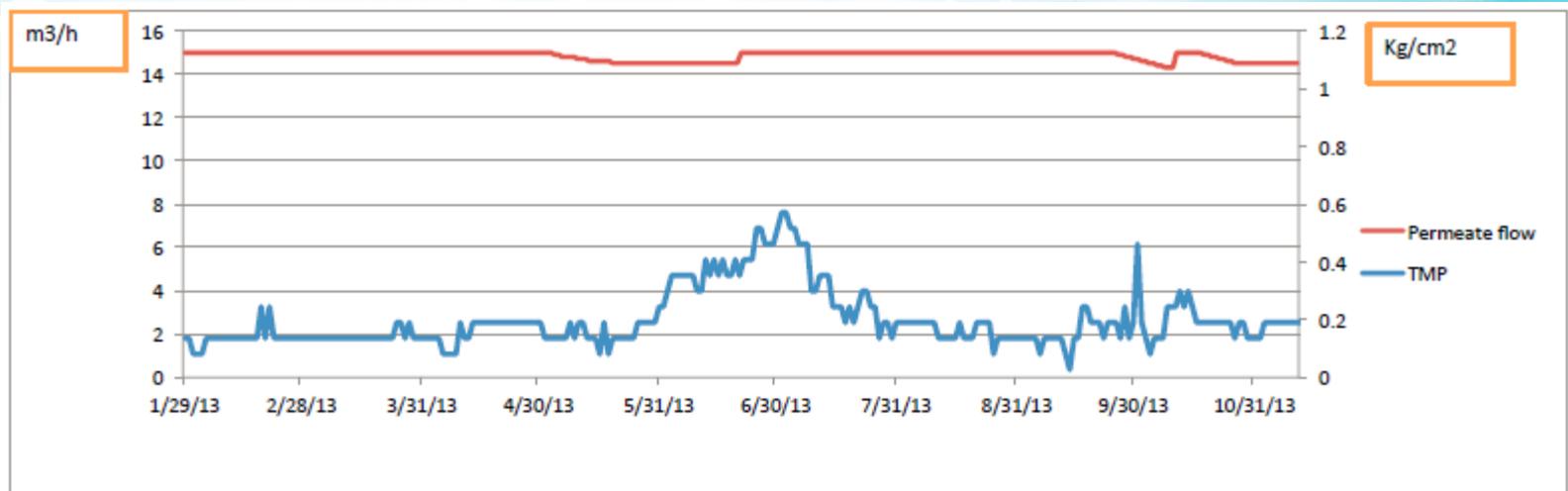


System 1 – Physical Cleaning Process

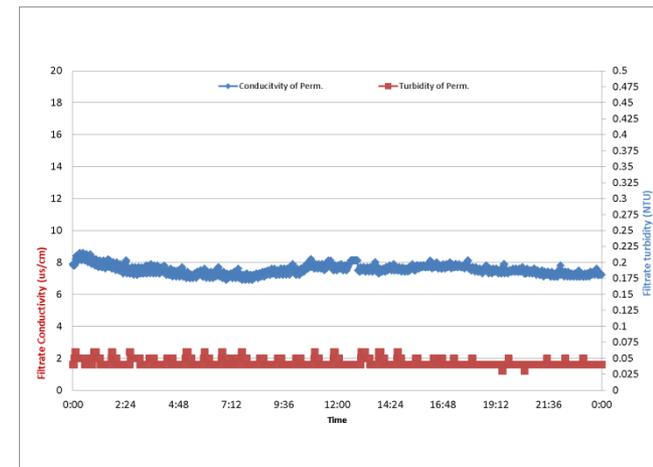
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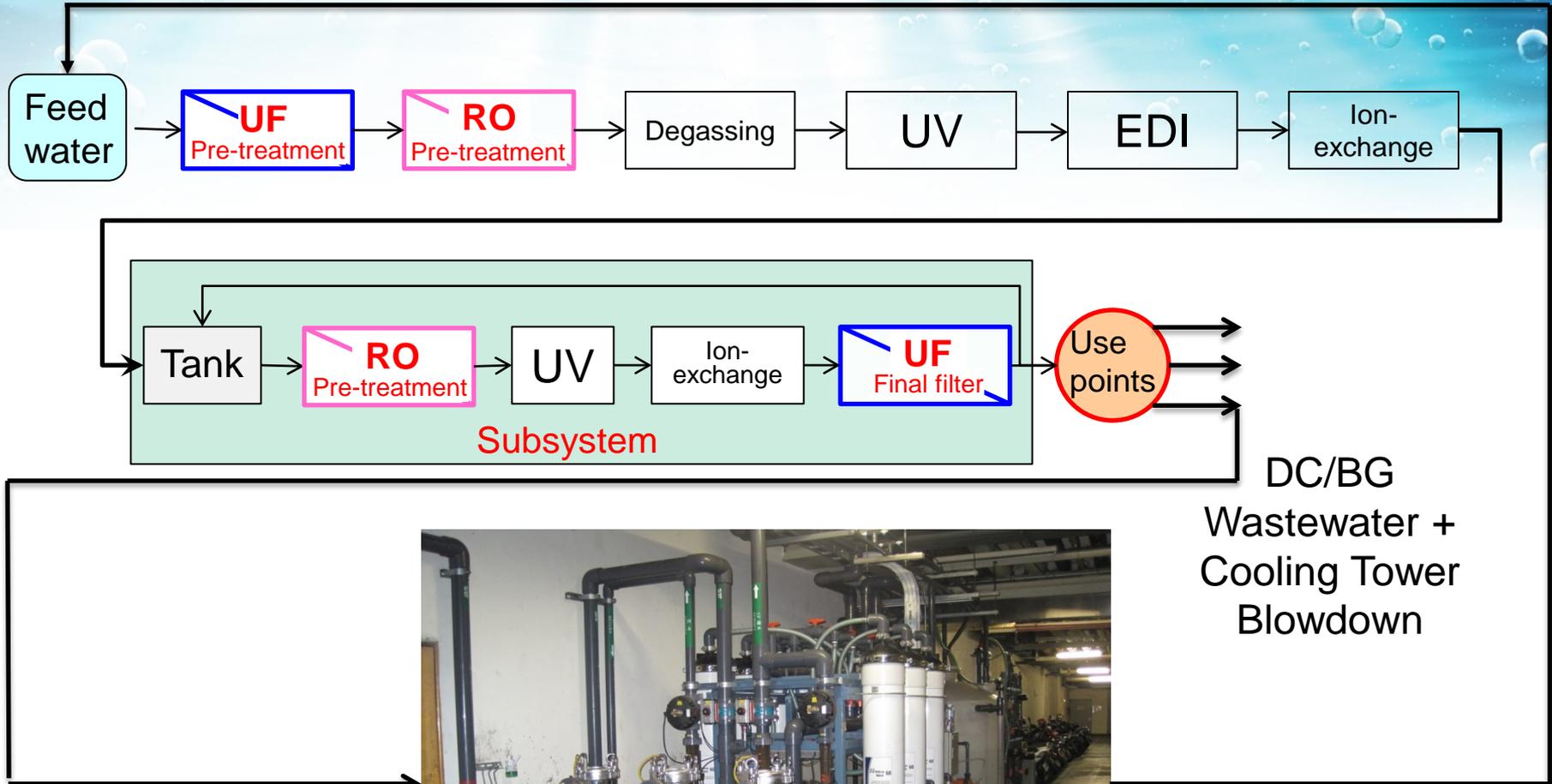
System 1 – Operating Performance



- Flux ~ 20 gfd
- Stable TMP – Avg. 4 psi
- Consistent Filtrate Turbidity <0.075 NTU



System 2 Overview



2-5 ppm Chlorine

200 micron Filter

6 HYDRAcap
MAX 60

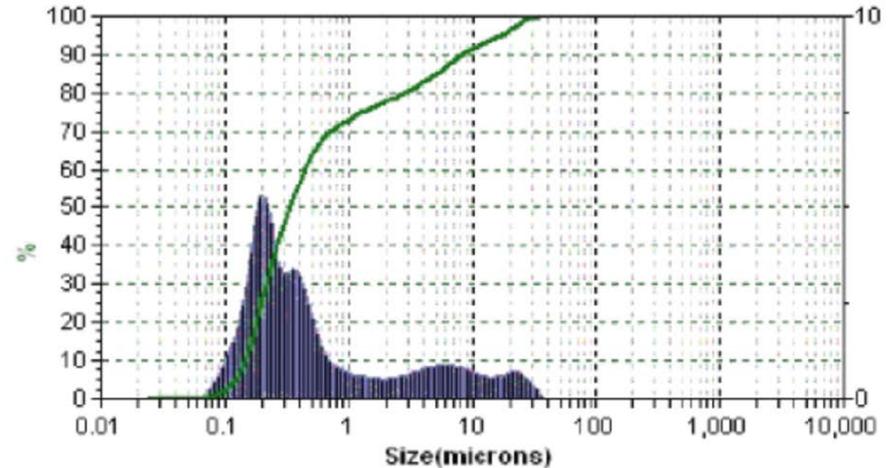
Case Study 2

Parameter	Unit	Value
System capacity	m3/day	432
Module type		Hydranautics HYDRAcap® MAX 60
Number of racks		1
Number of modules per rack		6
Gross operating filtration flux	LMH	35-40
Concentrate bleed flow	m3/hr	1.5
Filtration cycle duration	min	45
Physical cleaning method		Air scour with backwash
Air scour flow rate per module	m3/hr	4
Chemical cleaning frequency		Two caustic maintenance cleans per day (0.1% NaOH)
System Recovery	%	~85

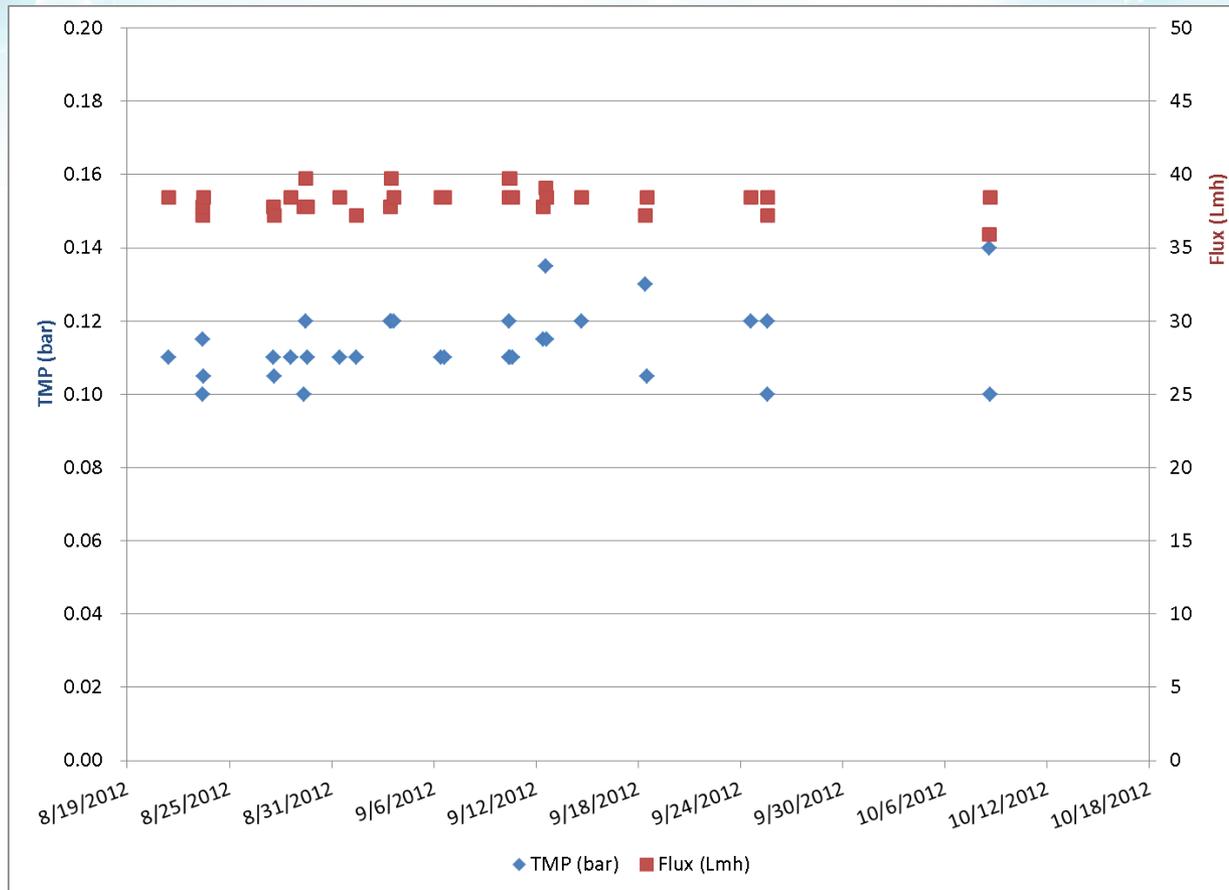


System 2 - Feed Water Quality

- Turbidity = 1100 NTU
- ~98% of particles larger than 0.1 micron



System 2 – Operating Performance



- Constant TMP ~ 2 psi
- 1st Year Filtrate Turbidity <0.1 NTU

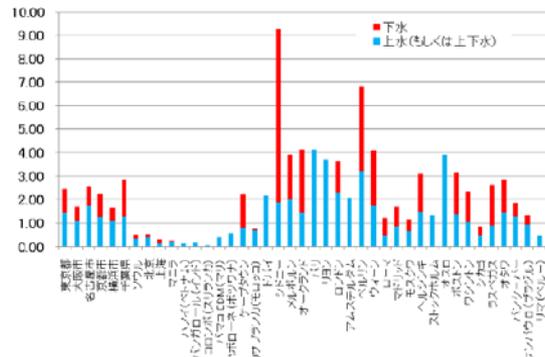
System 2 - Module Autopsy

- After ~1 year of operation, turbidity exceeded 0.1 NTU
- Tensiometry revealed slight strength decline
 - Most likely due to improper draining



System Cost Comparison

	Without Reuse	With Reuse – BW Free Operation (System 1)	With Reuse – Operation with BW (System 2)
Source Water and Sewer Cost - \$/mo.	8,140.31	1,866.24	2,214.80
Chem Cost - \$/mo.		128.65	128.65
Energy Cost - \$/mo		129.60	129.60
Operator - \$/mo		1,200.00	1,200.00
Total (\$/mo)	8,140.31	3,324.50	3,673.06
Difference (\$/mo)		4,815.81	4,467.25
System Cost		< \$150,000	\$150,000
Simple Payback Period		< 31 months	33.6 months



Conclusions

- Backwash free operation is capable of sustaining stable permeability, even when treating very high feed water turbidity
- Advantages of BW free system
 - Reduced OPEX through increased recovery
 - Reduced CAPEX through elimination of BW pump, tank, associated piping
- Proper drain piping arrangement critical

Conclusions

- BG/DC WW can be segregated from other use point wastewaters to optimize reuse potential and reduce CAPEX of primary UPW system by decreased equipment sizing
- Test operation without concentrate bleed
 - Payback period reduced by ~0.5 months for every 1% increase in recovery